



# PIPENET™ NEWS

VOLUME 2 . ISSUE 5 Summer - 2008

LEADING THE WAY IN FLUID FLOW ANALYSIS

## Welcome to the PIPENET e-newsletter!

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### NEWS!

**PIPENET** Vision 1.32 is now available!

Download it from [www.sunrise-sys.com](http://www.sunrise-sys.com).

All **PIPENET** users with valid Maintenance, Updates and Support can register.

Visit the Registration Page of [www.sunrise-sys.com](http://www.sunrise-sys.com) and add the words 'Service Pack' in the comments box.

**Spray/Sprinkler Autolayout** is a new feature requested by Fire Protection experts. **Network modelling** is now astoundingly fast with a choice of instant tank configurations and general area protection. **Autolayout** is an automated schematic tool.

### PIPENET Vision 1.32 *out now*

Please see page 2 for full details of the exciting new range of feature additions and enhancements now available to **PIPENET** users.

Also included in this edition are further articles on how to make the most of your **PIPENET** software to avoid water hammer, or model pipe reductions.

Instant global editing will allow you to work rapidly and effectively as will the new **Spray/Sprinkler** auto layout facility.

Don't forget that previous editions packed with news and advice can be found on our website [www.sunrise-sys.com](http://www.sunrise-sys.com)

## PIPENET Vision 1.32 *includes...*

### New features in **PIPENET Vision 1.32** in the **Graphical User Interface**

- **Spray/Sprinkler Autolayout** facilitates the rapid layout of nozzles for a choice of tank configurations and general area protection.
- **Improved display of characters**, particularly superscripts, in Far Eastern languages, for example, Chinese or Korean.
- **Maximum number of Spray/Sprinkler nozzle types** increased from 50 to 150 in the PIPENET library.
- **Transient Switch Components** now allow the use of mass flow units.
- **The Transient check valve** now uses a pressure difference unit for the trigger pressure.
- **Standard and Spray/Sprinkler Modules** benefit from an improved display of internal node pressure specification in the results files.
- **Improved range of font sizes** and line thickness available for the schematic.

### New features in **PIPENET Vision 1.32** in the **Calculator**

- **Standard and Spray/Sprinkler Modules** have an improved fan/filter model with reverse flow.
- **The Transient Module** calculator benefits from an improved interior position calculation in the pipe for the pressure extreme.
- **Transient Vacuum Breaker Model** is improved. The diameter of the air inlet valve can be zero to become a pure air release valve.

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## How can AUTOCAD be imported and exported into **PIPENET Vision**?

1. Import the AutoCAD drawing (such as a plot, plan or general arrangement drawing) into **PIPENET** as a .wmf or .dxf file.
2. Draw the **PIPENET** schematic on top of the imported drawing.
3. Optimise the **PIPENET** design and perform the necessary calculations.

4. This new schematic and other data are exported to AutoCAD by choosing from the **PIPENET** tool bar, **tools**, **'export to .dxf'** and finalising the exported schematic as a piping drawing.
5. Remember - the attribute data in **PIPENET** can be changed by the fire protection engineer if required.

# Global Editing in PIPENET Vision at the click of a mouse

1. This is the Data Window before the pipe type is selected:

	Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?
				in	m	m	in			m/sec	
1	1	4	5	12	10	0	0.0018	0	No pipe type	1260	YES
2	2	6	8	12	100	0	0.0018	0	No pipe type	1260	YES
3	3	8	9	10	50	0	0.0018	0	No pipe type	1260	NO
4	4	8	9	10	50	0	0.0018	0	No pipe type	1260	NO
5	5	9	10	12	100	0	0.0018	0	No pipe type	1260	YES
6	6	11	13	12	10	0	0.0018	0	No pipe type	1260	YES
7	8	13	15	12	20	0	0.0018	0	No pipe type	1260	NO
8	9	15	16	10	20	0	0.0018	0	No pipe type	1260	YES
9	10	15	17	12	20	0	0.0018	0	No pipe type	1260	NO
10	11	17	18	3	20	0	0.0018	0	No pipe type	1260	NO
11	12	17	19	12	20	0	0.0018	0	No pipe type	1260	NO
12	13	19	20	3	20	0	0.0018	0	No pipe type	1260	NO
13	14	19	21	12	20	0	0.0018	0	No pipe type	1260	NO
14	15	21	22	3	20	0	0.0018	0	No pipe type	1260	NO
15	16	21	23	12	20	0	0.0018	0	No pipe type	1260	NO
16	17	23	24	6	20	0	0.0018	0	No pipe type	1260	YES
17	18	23	25	12	20	0	0.0018	0	No pipe type	1260	NO
18	19	25	26	6	20	0	0.0018	0	No pipe type	1260	NO
19	20	25	27	6	40	0	0.0018	0	No pipe type	1260	NO
20	7	13	16	3	20	0	0.0018	0	No pipe type	1260	NO
21	21	16	18	12	20	0	0.0018	0	No pipe type	1260	NO
22	22	18	20	12	20	0	0.0018	0	No pipe type	1260	NO
23	23	20	22	12	20	0	0.0018	0	No pipe type	1260	NO
24	24	22	24	12	20	0	0.0018	0	No pipe type	1260	NO
25	25	24	26	12	20	0	0.0018	0	No pipe type	1260	NO
26	26	26	27	12	20	0	0.0018	0	No pipe type	1260	NO
27	27	27	14	12	50	0	0.0018	0	No pipe type	1260	YES

2. Select the pipe type for one pipe in the data window:

This assumes that the pipe type was selected in the **options menu** of PIPENET (after downloading the network from PDMS, which would not have had a pipe type)

Browse Pipe <span style="float: right;">Print</span>											
	Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?
				in	m	m	in			m/sec	
1	1	4	5	12	10	0	0.0018	0	No pipe type	1260	YES
2	2	6	8	12	100	0	0.0018	0	No pipe type	1260	YES
3	3	8	9	10	50	0	0.0018	0	AnsiB3610_40	1260	NO
4	4	8	9	10	50	0	0.0018	0	No pipe type	1260	NO

3. After selecting the pipe type, click on any cell other than the pipe type cell:

Browse Pipe <span style="float: right;">Print</span>											
D Data Graphs Result Graphs Tables Forces											
Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?	
			in	m	m	in			m/sec		
1	1	4	12	10	0	0.0018	0	AnsiB3610_40	1426.7	YES	
2	2	6	12	100	0	0.0018	0	No pipe type	1260	YES	

4. Click on the cell with the pipe type and make it active:

Browse Pipe <span style="float: right;">Print</span>											
D Data Graphs Result Graphs Tables Forces											
Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?	
			in	m	m	in			m/sec		
1	1	4	12	10	0	0.0018	0	AnsiB3610_40	1426.7	YES	
2	2	6	12	100	0	0.0018	0	No pipe type	1260	YES	

5. Right click on the cell and select paste in column:

Browse Pipe <span style="float: right;">Print</span>											
D Data Graphs Result Graphs Tables Forces											
Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?	
			in	m	m	in			m/sec		
1	1	4	12	10	0	0.0018	0	AnsiB3610_40	1426.7	YES	
2	2	6	12	100	0	0.0018	0	No pipe type			
3	3	8	10	50	0	0.0018	0	No pipe type			
4	4	8	10	50	0	0.0018	0	No pipe type			
5	5	9	12	100	0	0.0018	0	No pipe type	1260	YES	

6. Sit back and relax!!

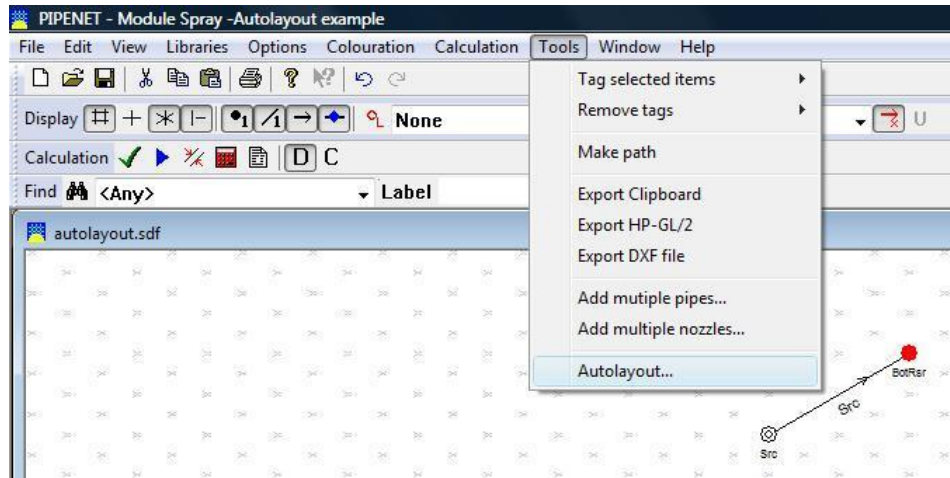
Browse Pipe <span style="float: right;">Print</span>											
D Data Graphs Result Graphs Tables Forces											
Label	Input node	Output node	Diameter	Length	Net height change	Roughness	Additional k-factor	Type	Wavespeed	Results selected?	
			in	m	m	in			m/sec		
1	1	4	12	10	0	0.0018	0	AnsiB3610_40	1426.7	YES	
2	2	6	12	100	0	0.0018	0	AnsiB3610_40	1426.7	YES	
3	3	8	10	50	0	0.0018	0	AnsiB3610_40	1436.11	NO	
4	4	8	10	50	0	0.0018	0	AnsiB3610_40	1436.11	NO	
5	5	9	12	100	0	0.0018	0	AnsiB3610_40	1426.7	YES	
6	6	11	12	10	0	0.0018	0	AnsiB3610_40	1426.7	YES	
7	8	13	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
8	9	15	10	20	0	0.0018	0	AnsiB3610_40	1436.11	YES	
9	10	15	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
10	11	17	12	20	0	0.0018	0	AnsiB3610_40	1502.01	NO	
11	12	17	3	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
12	13	19	3	20	0	0.0018	0	AnsiB3610_40	1502.01	NO	
13	14	19	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
14	15	21	3	20	0	0.0018	0	AnsiB3610_40	1502.01	NO	
15	16	21	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
16	17	23	6	20	0	0.0018	0	AnsiB3610_40	1463.93	YES	
17	18	23	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
18	19	25	6	20	0	0.0018	0	AnsiB3610_40	1463.93	NO	
19	20	25	6	40	0	0.0018	0	AnsiB3610_40	1463.93	NO	
20	7	13	3	20	0	0.0018	0	AnsiB3610_40	1502.01	NO	
21	21	16	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
22	22	18	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
23	23	20	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
24	24	22	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	
25	25	24	12	20	0	0.0018	0	AnsiB3610_40	1426.7	NO	

# Creating sprinkler networks using the Autolayout tool

The Autolayout tool, available in the PIPENET spray/sprinkler module, automates the task of designing spray/sprinkler systems for vessels or for area protection. Autolayout accelerates the design process!

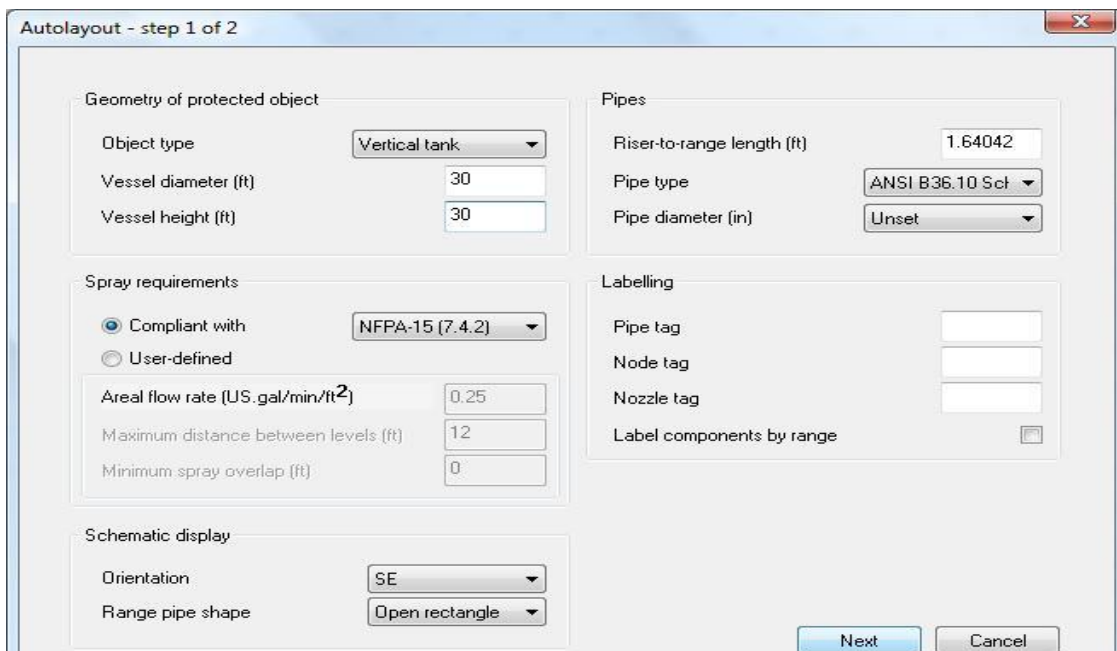
## 1. Launching Autolayout

- 1a. Select pipe types and nozzle libraries,
- 1b. Select Autolayout from the Tools menu bar item:



If an existing node is selected when the tool is launched, it will offer to join the new sub-network which is about to be generated to that node.

## 2. Dimensions and spray requirements



2. Specify the **shape** and **size** of the object to be protected, **spray density** and **nozzle layout** requirements (which can be selected to be compliant with a built-in fire-authority standard), **pipe parameters**, and **component labels**.

In the example on page 5, the diameter and height of the vessel were entered but all other parameters were left at their default values

### 3. Nozzle configuration

This makes it very easy to compare different nozzles in order to optimize the network according to your design criteria

Nozzle Type	Nozzles/range	Pressure	Flow/nozzle	Total nozzles	Total flow	Overlap
		psi A	US.gal/min		US.gal/min	ft
BETE-N3W	27	34.69595	15.37	81	1245.27	0.00103
BETE-N4	69	34.69595	22.44	207	4645.52	0.00654
BETE-N5	27	34.69595	30.75	81	2490.55	0.00103
HOSEREEL						
BETE-N2	11	162.56174	21.42	33	706.86	4.86479
Wall Drench-4	27	36.45161	18.85	81	1526.52	0.00103

Selected nozzle parameters

Spray cone angle (deg)

K-factor (US.gal/min,psi<sup>1/2</sup>)

Minimum/maximum pressure (psi A)

Minimum/maximum flowrate (US.gal/min)

Nozzle configuration

Nozzle-to-vessel distance (ft)

Minimum spray overlap (ft)

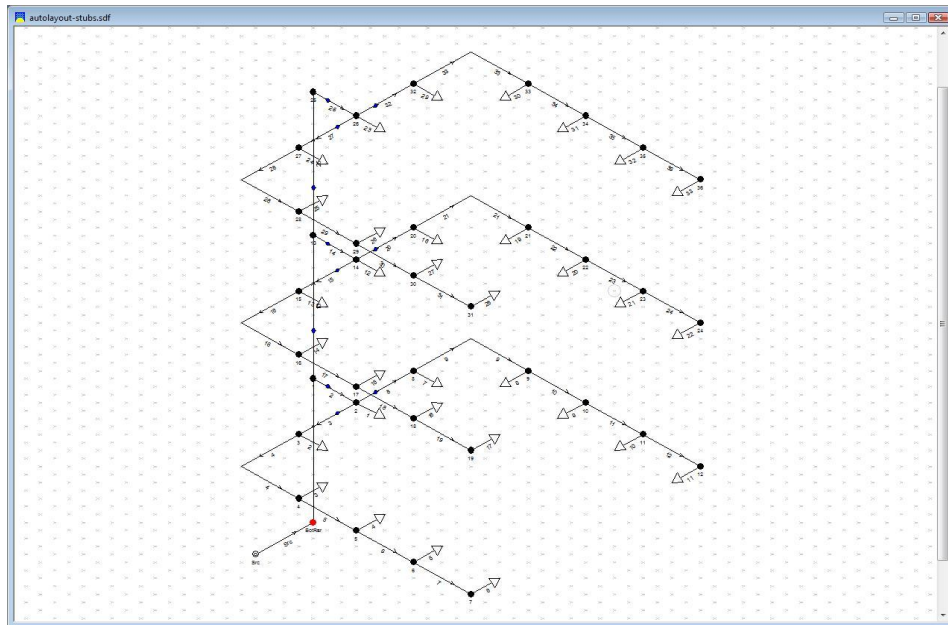
Number of sprinkler levels

Select the required nozzle from the list, and adjust the nozzle configuration if required. Next, click the Finish button!

### The generated Layout

The generated sub-network appears on the schematic grid ready for further editing!

All the generated pipes have appropriate elevations and fittings, and pipe-sizing can be performed in the usual way if the pipe diameter was left at its default value of  $\%Inset$  in the first dialogue.



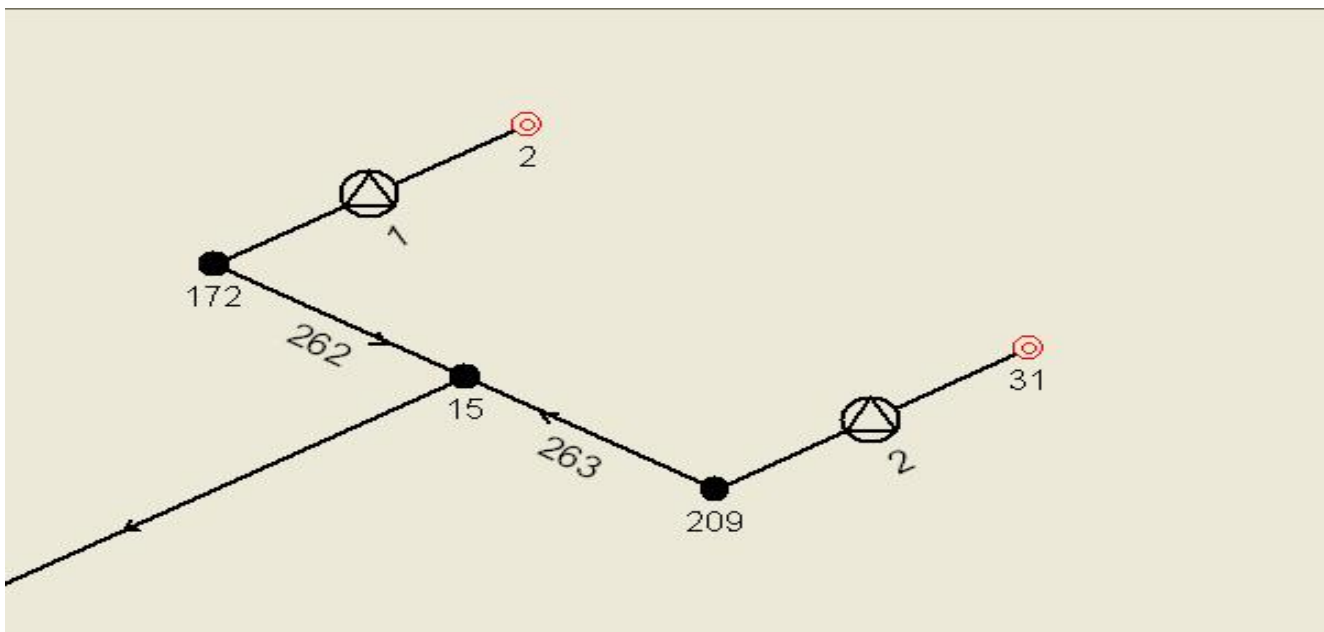
Seven mouse-clicks and the entry of two numbers generated this example!

## Modelling a Network with Two Inputs Combining Into One Single Pipe with PIPENET Vision

Normally, the inlet pressures of the pumps are known. The pumps will pump as much water as they can through the nozzles. The question is usually:

**How much water will flow through the nozzles when two pumps are working?**

In this example the inlet pressures of the pumps are both 0 bar G. The modelling can be done as follows:



Label	31	
Elevation	-16.5	m
Input/Output node	Input	
Design Spec.	NO	
Analysis Spec.	YES	
Pressure	0	kg/cm <sup>2</sup> G
Flow	Unset	l/min
<b>Results</b>		
Pressure	n/a	
Flow Rate	n/a	

Label	2	
Elevation	-22.5	m
Input/Output node	Input	
Design Spec.	YES	
Flow	5172.9	l/min
Analysis Spec.	YES	
Pressure	0	kg/cm <sup>2</sup> G
Flow	Unset	l/min
<b>Results</b>		
Pressure	n/a	
Flow Rate	n/a	

**Network Options**

Title Spray Options Units Pipe types Display Calculation Tables Defaults

Number of Lines per Page: 55  
 Max. Number of Iterations: 50  
 Convergence Accuracy: 0.001  
 Height Check Tolerance (m): 0.5

**Specifications**

Remote nozzle specifications  
 Mass balance specifications  
 User-defined specifications

**Nozzle specification**

Nozzle label:   
 Flowrate (l/min):

Note that only one nozzle specification may be supplied, and only when the User-defined specifications option is selected.

Temporary path: C:\Temp

Defaults

OK Cancel Apply

Browse Node Print

Data Results Graphs

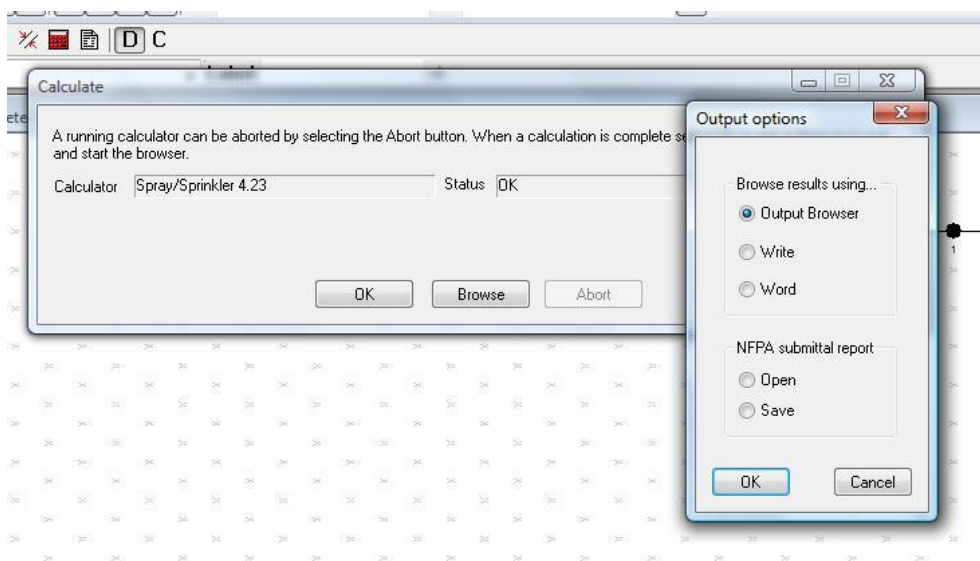
	L...	Elevation	Input/Output node	Design Spec.	Analysis Spec.	Pressure	Flow Rate
		m				kg/cm <sup>2</sup> G	l/min
1	1	-23	No	NO	NO	11.768	n/a
2	2	-22.5	Input	YES	YES	0	6600.7
3	3	-24	No	NO	NO	11.851	n/a
4	4	-23	No	NO	NO	11.773	n/a
5	5	-23	No	NO	NO	11.776	n/a
6	6	-23	No	NO	NO	11.78	n/a
7	7	-23	No	NO	NO	11.785	n/a
8	8	-20.5	No	NO	NO	11.538	n/a
9	9	-17	No	NO	NO	11.159	n/a
10	10	-15	No	NO	NO	10.931	n/a
11	11	-15	No	NO	NO	10.939	n/a
12	12	-15	No	NO	NO	10.937	n/a
13	13	-15	No	NO	NO	10.925	n/a
14	14	-22.5	No	NO	NO	11.773	n/a
15	15	-19.5	No	NO	NO	11.488	n/a
16	16	-15	No	NO	NO	10.917	n/a
17	17	0	No	NO	NO	9.369	n/a
18	18	8	No	NO	NO	8.421	n/a
19	19	8	No	NO	NO	6.666	n/a
20	20	3	No	NO	NO	6.935	n/a
21	21	8	No	NO	NO	8.417	n/a
22	22	8	No	NO	NO	6.679	n/a
23	23	3	No	NO	NO	6.986	n/a
24	24	8	No	NO	NO	8.416	n/a
25	25	8	No	NO	NO	6.672	n/a
26	26	3	No	NO	NO	6.978	n/a
27	27	8	No	NO	NO	8.415	n/a
28	28	8	No	NO	NO	6.66	n/a
29	29	3	No	NO	NO	6.929	n/a
30	30	3	No	NO	NO	6.592	n/a
31	31	-16.5	Input	NO	YES	0	8433.5
32	32	-22	No	NO	NO	7.598	n/a

It is also possible, but not advisable for good design, to perform the calculation by using the most remote nozzle option.

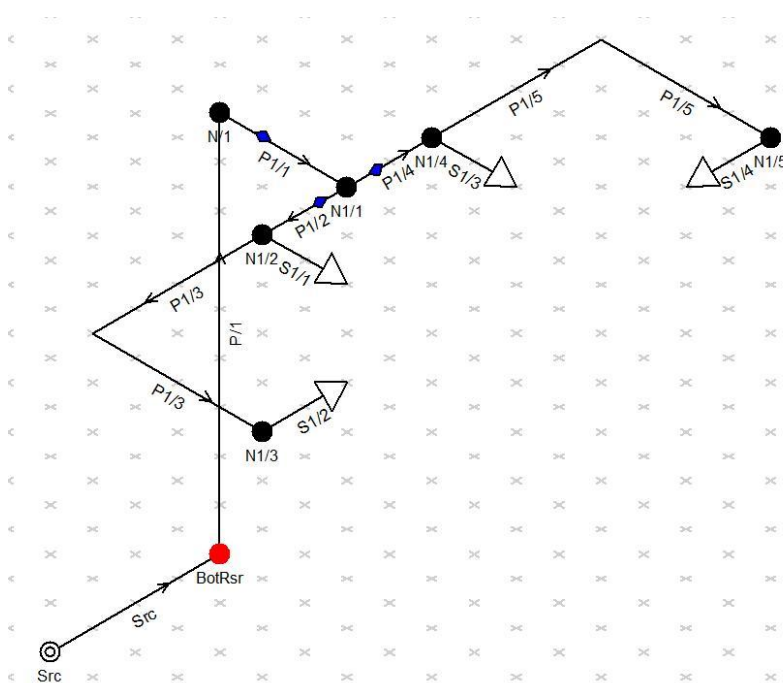
## Generating tables for an NFPA report

In the PIPENET Spray/Sprinkler module, hydraulic calculation details can now be written to a file in tabular form in order to assist in the preparation of a fire protection submittal of the kind required by the NFPA. The output file is written in rich text format. The calculation results are presented in the form of **Node analysis** and **Pipe information** tables, which are designed to comply with the format specified in the 2007 Edition of NFPA-13 and are suitable for inclusion in a submittal report.

This new facility is made available through additional options in the browser dialogue, which can be opened from the calculate dialogue or the calculation toolbar:



By way of illustration, the tables generated for the following simple network are shown below:



## Summary Values

<b>Title</b>	NFPA Example
<b>Calculation date</b>	24-Sep-2008 11:23
<b>Calculator</b>	PIPENET Vision Spray calculator, version 4.23
<b>Friction loss formula</b>	Hazen-Williams
<b>Design standard</b>	NFPA 1996/2001
<b>Total number of sprinkler heads</b>	4
<b>Number of sprinkler heads on</b>	4
<b>Total sprinkler discharge (US.gal/min)</b>	56.825
<b>Total non-sprinkler output flow (US.gal/min)</b>	0.000
<b>Total input flow (US.gal/min)</b>	56.825
<b>Highest fluid velocity (ft/sec)</b>	8.955
<b>Pressure at input nodes</b>	See NODE ANALYSIS table

## Node Analysis

<b>Node tag</b>	<b>Elevation (ft)</b>	<b>Node Type</b>	<b>Pressure (psi A)</b>	<b>Discharge (US.gal/min)</b>	<b>Notes</b>
BOTRSR/0	0.00		94.422	0.000	
N/1	12.00		87.891	0.000	
N1/1	12.00		87.262	0.000	
N1/2	12.00	Sprinkler	86.869	14.272	Nozzle label: S1/1
N1/3	12.00	Sprinkler	85.536	14.140	Nozzle label: S1/2
N1/4	12.00	Sprinkler	86.869	14.272	Nozzle label: S1/3
N1/5	12.00	Sprinkler	85.536	14.140	Nozzle label: S1/4
SRC/0	0.00	Input	95.538	0.000	

## Pipe Information

Node 1	Elev 1 (ft)	K factor	Flow added (q) (US.gal/min)	Nominal ID (inches)	Fittings - quantity, type, and equivalent length (ft)	L (ft)	C factor	Pt (psi A)	Notes
BOTRSR/0	0.00			1.5		12.001	120.0	73.195	Vel = 8.955 ft/sec
						0.000		-5.193	
N/1	12.00	P/1	56.825	1.610		12.001	0.112	1.338	
N/1	12.00			1.5	1xE=4.00	1.640	120.0	72.566	Vel = 8.955 ft/sec
						3.999		0.000	
N1/1	12.00	P1/1	56.825	1.610		5.640	0.112	0.629	
N1/1	12.00	1.68		1.25	1xE=3.00	3.000	120.0	72.173	Vel = 6.095 ft/sec
						3.000		0.000	
N1/2	12.00	P1/2 S1/1	28.412	1.380		6.000	0.066	0.393	
N1/2	12.00	1.68		0.75		6.001	120.0	70.840	Vel = 8.507 ft/sec
						0.000		0.000	
N1/3	12.00	P1/3 S1/2	14.140	0.824		6.001	0.222	1.332	
N1/1	12.00	1.68		1.25	1xE=3.00	3.000	120.0	72.173	Vel = 6.095 ft/sec
						3.000		0.000	
N1/4	12.00	P1/4 S1/3	28.412	1.380		6.000	0.066	0.393	
N1/4	12.00	1.68		0.75		6.001	120.0	70.840	Vel = 8.507 ft/sec
						0.000		0.000	
N1/5	12.00	P1/5 S1/4	14.140	0.824		6.001	0.222	1.332	
SRC/0	0.00		56.825	1.5		10.000	120.0	79.726	Vel = 8.955 ft/sec
						0.000		0.000	
BOTRSR/0	0.00	SRC/0	56.825	1.610		10.000	0.112	1.115	

# Solving Liquid Hammer Problems, Using PIPENET and CAESAR II

By: Farhad Salehi of Alpha Afzaar Inc.

## Liquid hammer - A Destructive force

Liquid hammer is the destructive force causing pounding noises and vibration in a piping system when liquid flowing through a pipeline is stopped abruptly. When sudden changes in flow occur, the energy associated with the flowing liquid is suddenly transformed into pressure at that location. This excess pressure is known as surge pressure and is greater with large changes in velocity. Characteristics of the pipe such as the materials used in construction, the wall thickness, and the temperature of the pipe, all affect the elastic properties of the pipe and how it will respond to surge pressures.

The thicker pipe wall and stronger pipes and fittings the faster the shock wave. Thin walled plastic pipe will only bounce a shock wave back at 914 m/s while heavy wall steel pipe will bounce a shock wave back at 2438 m/s.

Liquid does not actually travel down a pipe line at these speeds. For example 1.5 to 2 meters per second is very fast for water to flow in a pipeline. A pressure wave or shock wave in liquid happens when one liquid molecule pushes on another liquid molecule and the second molecule pushes on a third and so on. If you have a pipeline 1,000 meters long full of water, injecting a thimble full of water in one end of the pipe will cause another thimble of water to almost instantaneously come out of the other end of the pipe. The non compressible nature of most liquids is what transmits a shock wave through pipelines at such unimaginable speeds. Stronger or thicker walled pipe and fittings are better able to withstand the repeated impacts of liquid hammer but, as the strength of the pipe and fittings increases, the velocity of the shock wave increases causing more damage.

## Causes of Liquid Hammer

The causes of liquid hammer are varied. There are, however, four common events that typically induce large changes in pressure:

1. Pump start-up can induce the rapid collapse of a void space that exists downstream from a starting pump. This generates high pressures.
2. Pump power failure can create a rapid change in flow, which causes a pressure up-surge on the suction side and a pressure down-surge on the discharge side. The down-surge is usually the major problem. The pressure on the discharge side reaches vapour pressure, resulting in vapour column separation.
3. Valve opening and closing is fundamental to safe pipeline operation. Closing a valve at the downstream end of a pipeline creates a pressure wave that moves toward the reservoir. Closing a valve in less time than it takes for the pressure surge to travel to the end of the pipeline and back is

called **sudden valve closure**. Sudden valve closure will change velocity quickly and can result in a pressure surge. The pressure surge resulting from a sudden valve opening is usually not as excessive.

- Improper operation or incorporation of surge protection devices can do more harm than good. An example is over sizing the surge relief valve or improperly selecting the vacuum breaker-air relief valve. Another example is to try to incorporate some means of preventing liquid hammer when it may not be a problem.

### Manual Load Calculation

$$dp = \rho \cdot c \cdot dv$$

Where:

- dp** . is the pressure rise due to the fluid's instantaneous stopping.
- ρ** . is the fluid density.
- c** . is the speed of sound in the fluid.
- dv** . is the change in velocity of the fluid.

The speed of sound in the fluid can be estimated from:

$$c = [E_f / (\rho + \rho(E_f / E) (d/t) )]^{0.5}$$

Where:

- E<sub>f</sub>** . is the bulk modulus of the fluid.
- E** . is the modulus of elasticity of the pipe.
- d** . is the pipe mean diameter.
- t** . is the pipe wall thickness.
- ρ** . is the fluid density.

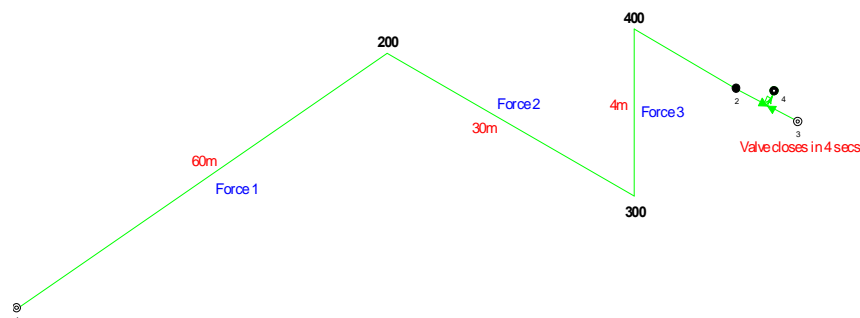
The magnitude of unbalanced load can be computed from:

$$F = dp \cdot \text{Area}$$

### PIPENET Model

In the following example, the water hammer phenomenon happens when the stop valve closes in 4 seconds.

**PIPENET** Transient simulates pressure surge in piping systems.



**Figure 1** . piping system for analysis - This is a 10 inch, Std. WT, A106-B pipe. Water is flowing through the pipe with 11.2 bar pressure and 20°C temperature. Suddenly, the valve closes in 4 seconds.

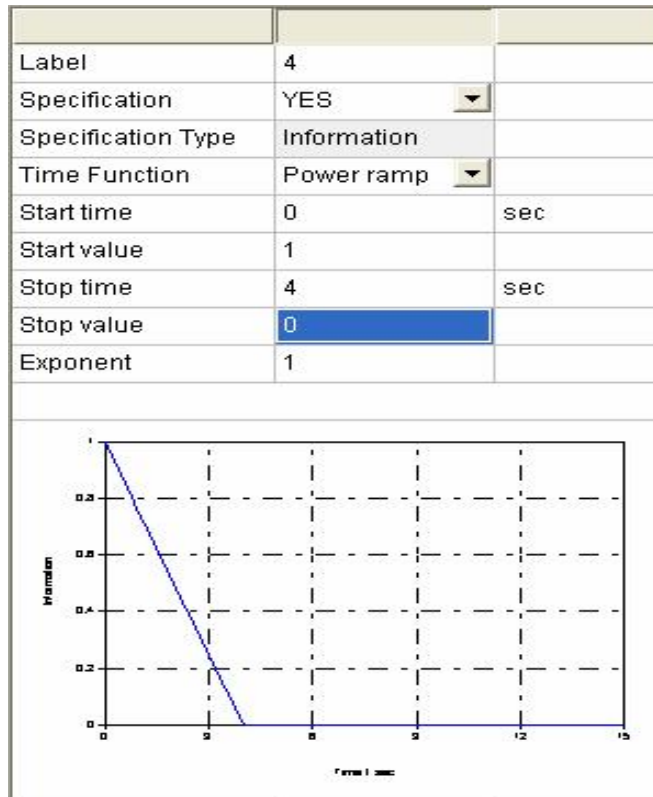


Figure 2 - the specification applied to valve closure with power-ramp time function.

It is most likely that the water hammer load will be found in segment 200-300 (force 2), shown in figure 1. The magnitude of applied dynamic force due to a pressure surge in elbow-elbow pair 200-300 is illustrated in figure 3 below. This load spectrum is a uni-axial force along the pipe. The direction must be specified in the CAESAR II dynamic model correctly, later.

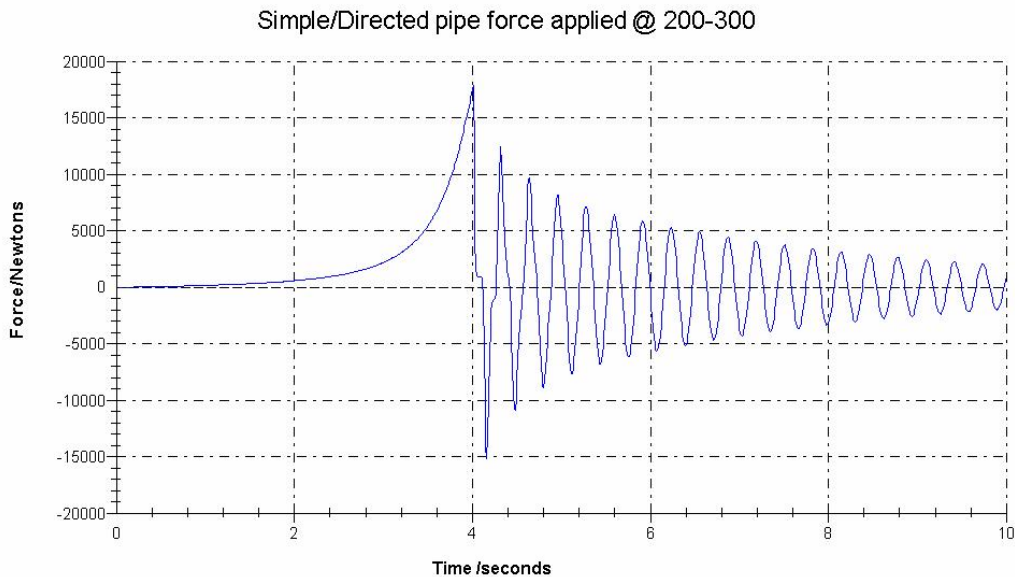


Figure 3

## CAESAR II Model:

After creating the same model in CAESAR II and performing static analysis shown in figure 4, we see that the support loads and the maximum stress are very low and acceptable. (Code Stress Ratio is 13.0 at Node 410  
LOADCASE: 2 (SUS) W+P1)

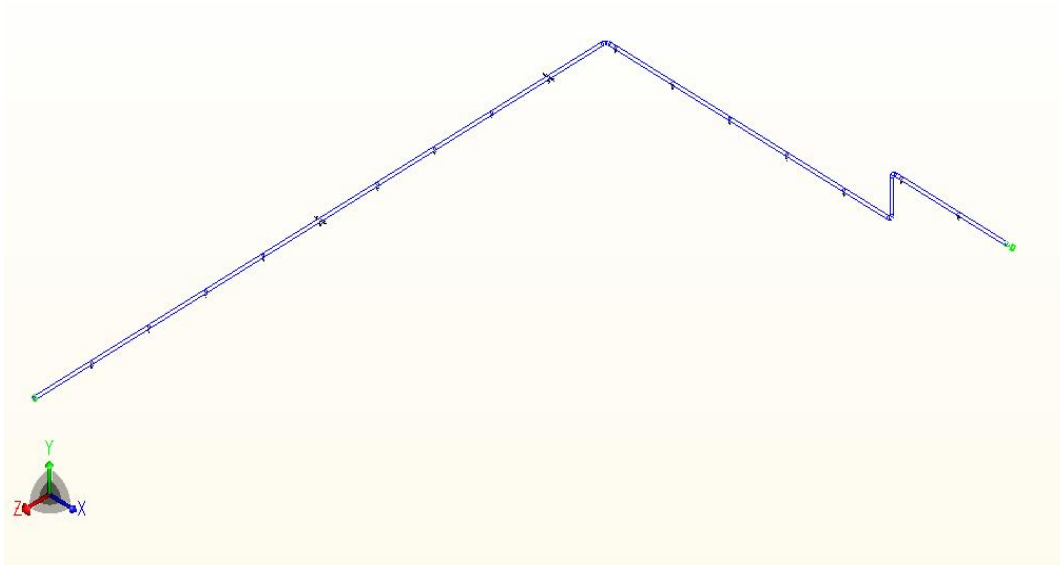


Figure 4

## PERFORMING DYNAMIC CALCULATION:

**PIPENET** creates an .FRC file for each defined force in the model. CAESAR II can read .FRC files and create a dynamic input file automatically. We can import an .FRC file in CAESAR II by using Tools>External Interfaces> **PIPENET** from CAESAR II main menu. After performing dynamic analysis, we'll see stress failure and excessive forces on some of the pipe supports shown below.

RESTRAINT REPORT, Loads on Restraints  
(OCC) COMBINATION # 1

NODE	-----Forces( N.)-----			-----Moments( N.m. )-----			
	FX	FY	FZ	MX	MY	MZ	
100	4140	2063	1451	2063	21443	23	Rigid ANC
250	0	14733	0	0	0	0	Rigid +Y
410	0	10935	0	0	0	0	Rigid +Y
600	13618	7591	1164	1308	8335	7723	Rigid ANC

\*\*\*\* B31.3 -2006, May 31, 2007

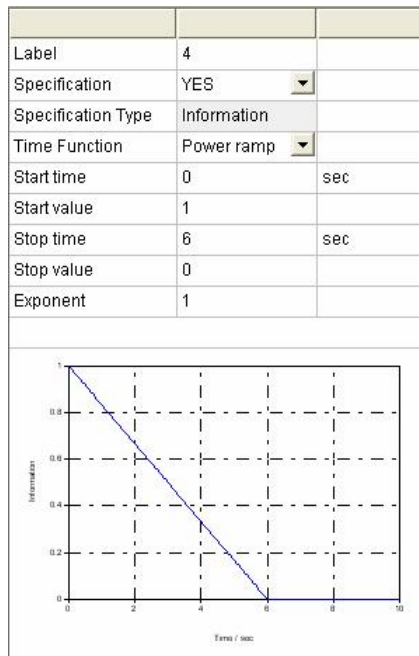
\*\*\*\* CODE STRESS CHECK FAILED

HIGHEST STRESSES: ( KPa )

CODE STRESS %:	106.1	@NODE	298
STRESS:	194578.8	ALLOWABLE:	183401.
BENDING STRESS:	183613.0	@NODE	298
TORSIONAL STRESS:	5011.1	@NODE	300
AXIAL STRESS:	11947.4	@NODE	298
3D MAX INTENSITY:	201337.9	@NODE	299

## The Fix

1. In long pipelines, surge can be relieved with a tank of water directly connected to the pipeline called a surge tank. When a surge is encountered, the tank will act to relieve the pressure, and can store excess liquid, giving the flow alternative storage better than that provided by expansion of the pipe wall and compression of the fluid. Surge tanks can serve for both positive and negative pressure fluctuations.
2. Air chambers are installed in areas where water hammer is encountered frequently, and are typically seen behind sink and tub fixtures. Shaped like thin, upside-down bottles with a small orifice connection to the pipe, they are air-filled. The air compresses to absorb the shock, protecting the fixture and piping.
3. In this situation, the best form of water hammer prevention is to have automatically-controlled valves, which close slowly. Closing the valve slowly can moderate the rise in the pressure when the down surge wave - resulting from the valve closing - returns from the source or reservoir.

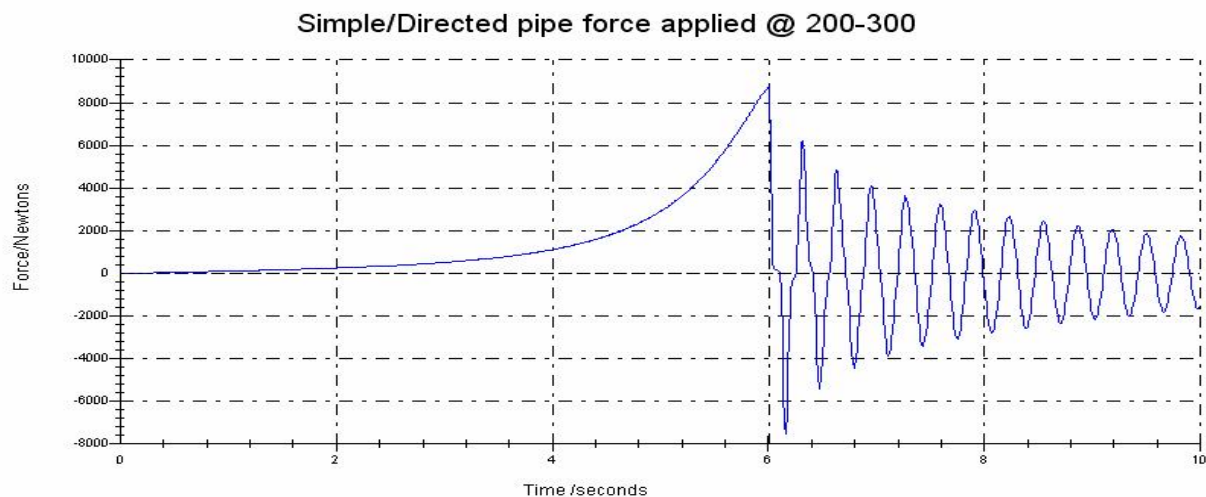


which close slowly. Closing the valve slowly can moderate the rise in the pressure when the down surge wave - resulting from the valve closing - returns from the source or reservoir.

Going back to the **PIPENET** model and changing the valve closure time to 6 sec. (figure 5) will cause fewer water hammer loads, as shown in figure 6.

**Figure 5**

**NOTE:** Lower values of the exponent cause the majority of the flow cut off to occur at the end of closure, while larger values of the closure exponent cause the majority of flow cut off to occur at the beginning of closure.



**Figure 6**

Now, dynamic analysis is performed for this model again with the new .FRC file. At this time, support loads are far better than in the previous situation and the code stress also passed as shown below.

RESTRAINT REPORT, Loads on Restraints  
(OCC) COMBINATION # 1

NODE	-----Forces( N.)-----			-----Moments( N.m. )-----			
	FX	FY	FZ	MX	MY	MZ	
100	1991	2063	701	2063	10648	18	Rigid ANC
250	0	9607	0	0	0	0	Rigid +Y
410	0	8885	0	0	0	0	Rigid +Y
600	6844	6824	584	680	4230	5943	Rigid ANC

\*\*\*\* B31.3 -2006, May 31, 2007  
\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: ( KPa )  
CODE STRESS %: 57.0 @NODE 298  
STRESS: 104517.9 ALLOWABLE: 183401.  
BENDING STRESS: 94708.5 @NODE 298  
TORSIONAL STRESS: 2521.1 @NODE 300  
AXIAL STRESS: 10331.8 @NODE 399  
3D MAX INTENSITY: 110781.1 @NODE 299

## Conclusion

Liquid hammer will continue to pose a challenge because it is associated with systems that cannot be exactly defined. By knowing how to avoid situations that will create liquid hammer, a lot of problems with failed valves and equipment and costly downtime can be avoided.

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## PIPENET NEWS

If you would like to be added to the **PIPENET NEWS** circulation list, please email: [sales@sunrise-sys.com](mailto:sales@sunrise-sys.com).  
(If you would prefer to be removed from the circulation list, please email ~~to~~ to the same address. Thank you.)

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## PIPENET Demonstration

Do you want to know more about **PIPENET**? Are you looking for a demonstration? Visit the registration page of [www.sunrise-sys.com](http://www.sunrise-sys.com) and ask to see the new **PIPENET** Vision demonstration of all three modules.

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**LEADING THE WAY IN FLUID FLOW ANALYSIS**

## PIPENET VISION 1.40

Our Development Team is currently working towards **PIPENET Vision 1.40**. It will incorporate even more features requested by our users, including more options on autolayout and **even better presentation of results**. If you would like to comment, please contact us by emailing [sales@sunrise-sys.com](mailto:sales@sunrise-sys.com).

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## PIPENET Maintenance Updates and Support Subscription

For a small annual subscription you can ensure that you are always working with the latest version of **PIPENET**, as well as being assured of assistance from our support. Email [sales@sunrise-sys.com](mailto:sales@sunrise-sys.com) for more information.

**PIPENET Vision 1.40** will be sent, free of charge to all customers with a valid Maintenance, Updates and Support contract when it is released.

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**ISO 9001 Accreditation** - We are delighted that Sunrise Systems has been re-accredited once again!

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## PIPENET Marketing Partners

We are based in Cambridge in the UK, but we do have a team of excellent marketing partners across the globe. Visit us at [www.sunrise-sys.com](http://www.sunrise-sys.com). Register your address details and the application of interest to you and we will be pleased to give you the contact details of a marketing partner close to you.

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## PIPENET Customer Feedback

Please let us know what additional features you would like to enjoy in future versions of PIPENET. We value customer feedback and comments highly, so we will be very pleased to hear from you. Please give us your comments via the **Contact Us** page of our website [www.sunrise-sys.com](http://www.sunrise-sys.com).

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Don't forget to visit [www.sunrise-sys.com](http://www.sunrise-sys.com) for the latest **PIPENET Vision** news.



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